



Energikonvertering i fremtidens effektive energisystem

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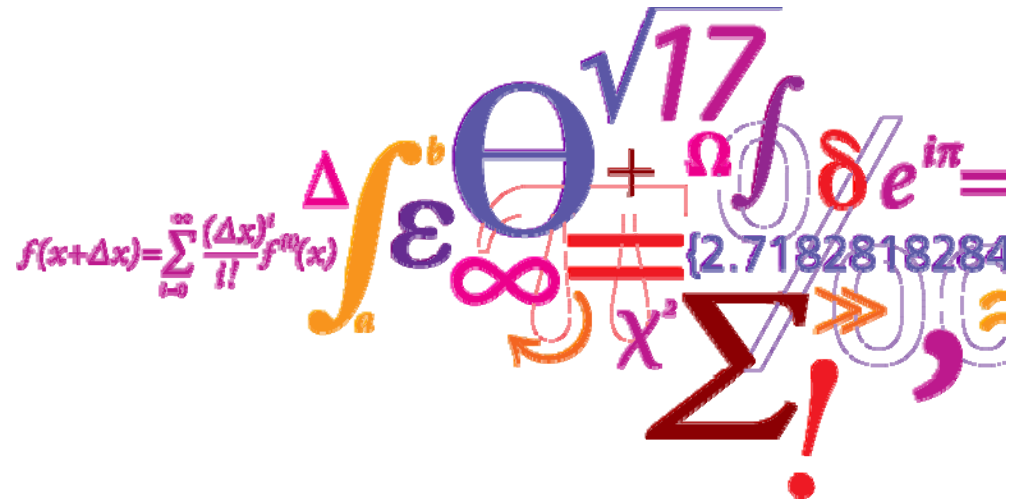
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Energikonvertering i fremtidens effektive energisystem

Peter V. Hendriksen, DTU Energikonvertering



Ændringer i Energisystemet, drivende faktorer

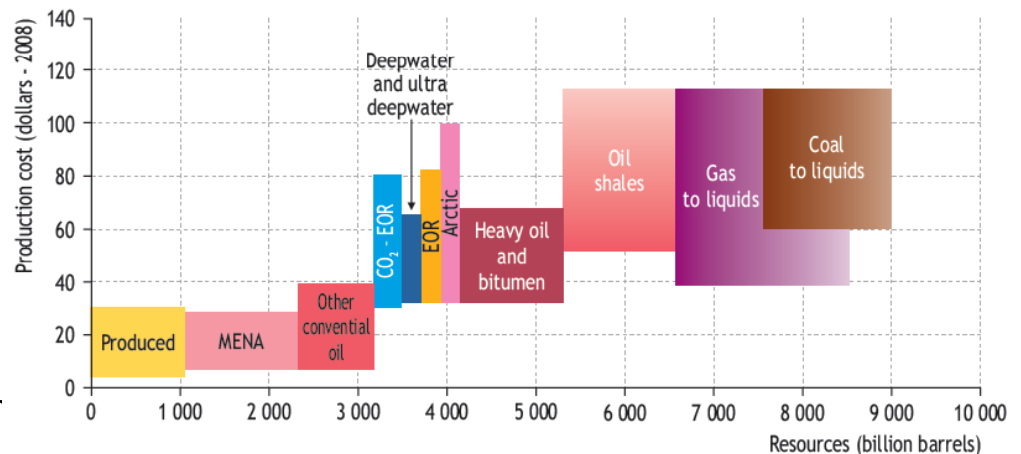
- Hensyn til klima, minimering af emissioner. 
- Forsyningssikkerhed 
- Økonomi, Pris på konventionelle fossile brændsler 
- Erhvervspolitik
- Accept/manglende accept af atomkraft 
- Geopolitiske, strategiske hensyn 
- Forøget forbrug, befolkningstilvækst 

• ..

• Ressourceknapped

- *store fossile ressourcer*
- *store vind/sol ressourcer*

Figure 9.10 • Long-term oil-supply cost curve

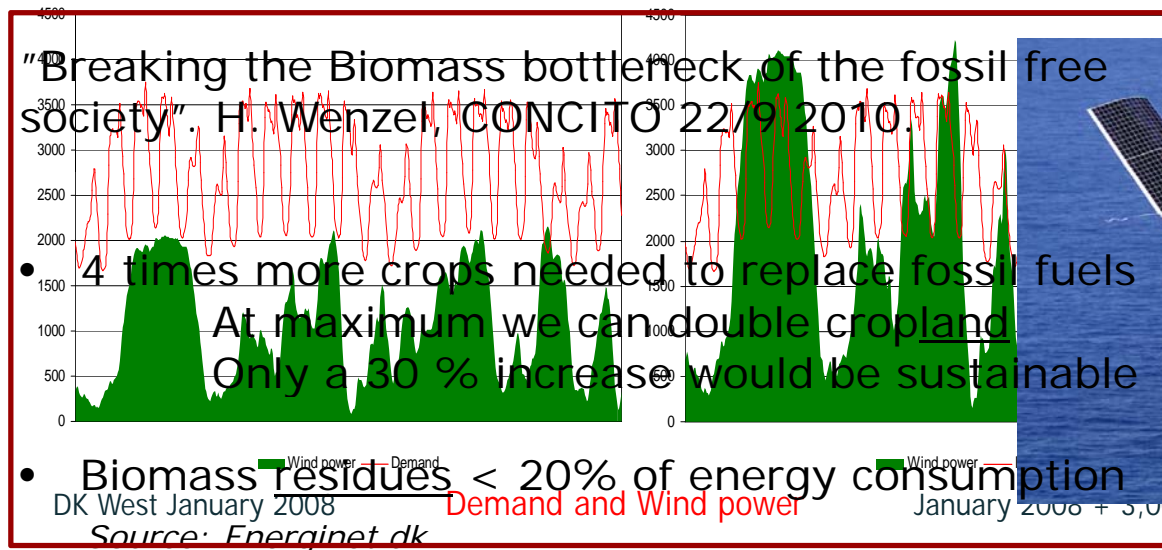


Dansk Målsætning

- 2020: 50 % El forbrug dækket af VE
- 2035: 0 % Fossil energi i el og varme -produktion
- 2050: 100 % VE

Udfordringer

1. Øget andel af fluktuerende produktion
2. Biomasse er en begrænset ressource !
3. Flydende brændstoffer (Fly, tung transport) hvorfra ?



"The role of fuel cells and electrolyzers in future efficient energy systems"

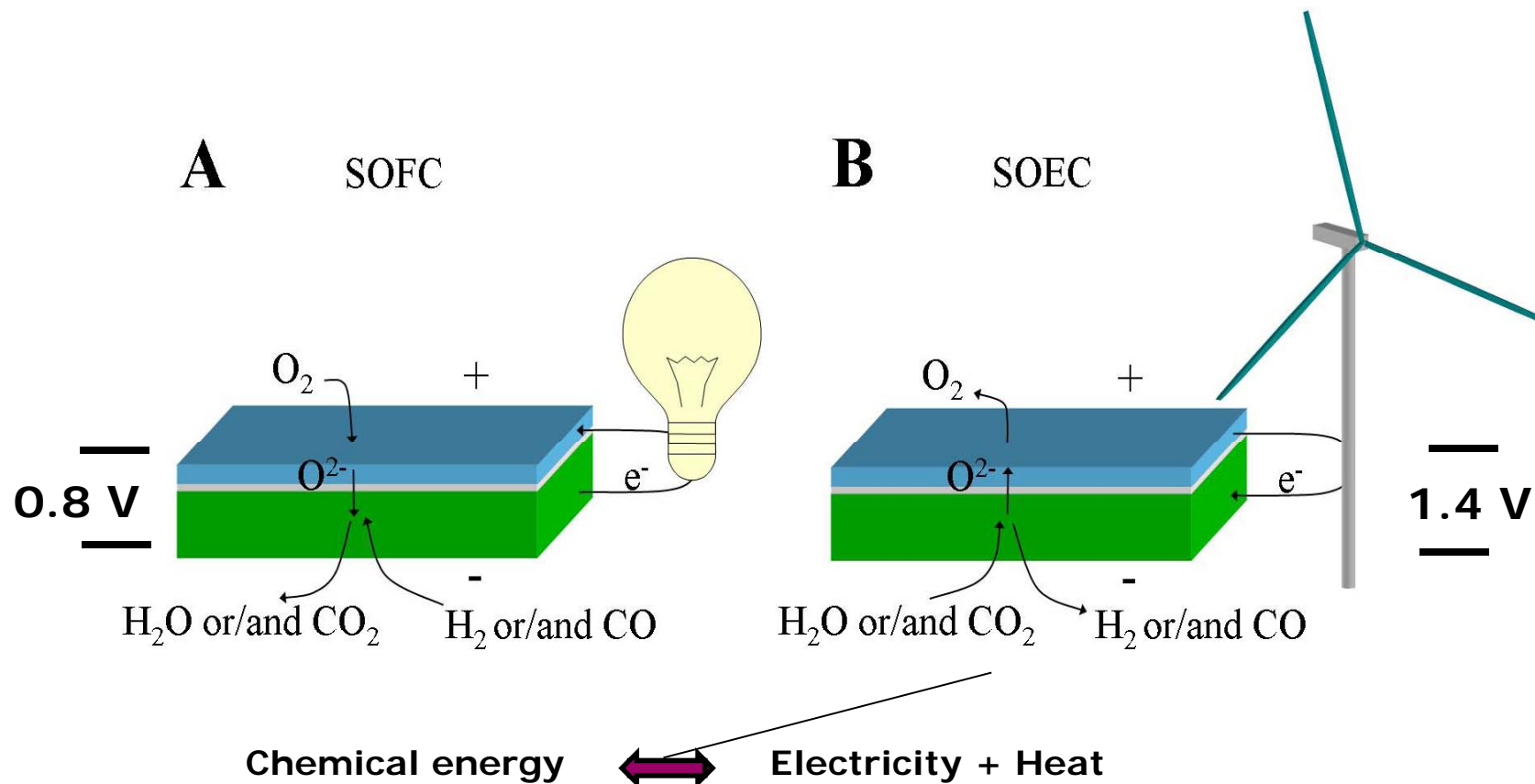
Peter Vang Hendriksen, DTU Energy Conversion,

Brian Vad Mathiesen, Department of Development and Planning, Aalborg University,

Allan S. Pedersen and Søren Linderøth, DTU Energy Conversion;

Ch13 DTU Energy Report. Enabling technologies

Brændselsceller og Elektrolyse kan bidrage til løsning !



Brug af brændselsceller i fremtidens energisystem

- Hvorfor ?
 - Høj el-virkningsgrad
 - God del-last karakteristik (virkningsgrad)
 - Fleksible
- Lokal CHP vha. brændselsceller
 - Minimerer transmissionstab
- Systemstudier viser at decentral FC-CHP er mere fordelagtigt
- Transport; FC-vehicles

~6 % i DK på el-siden (*Ref 1*)
 ~20% på fjernvarme (*Ref 2*)

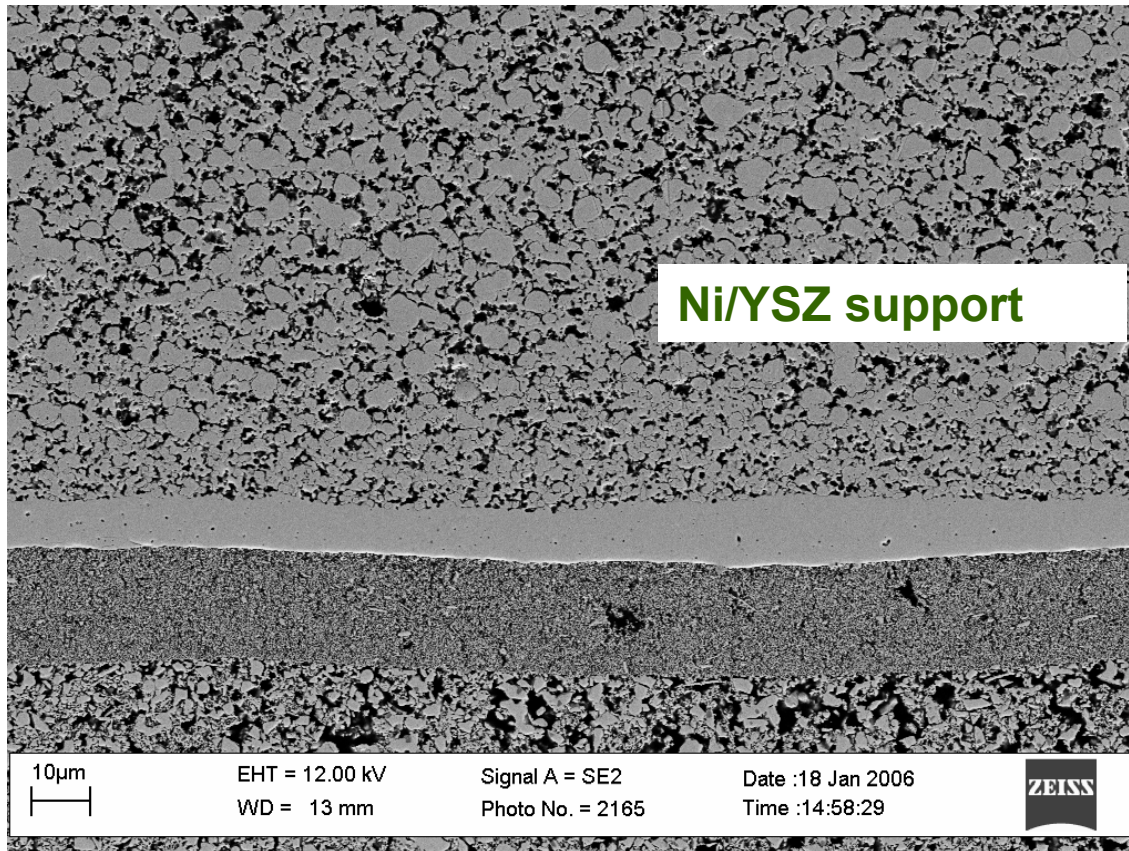
Større indpasning af varmepumper mulig (=brændselsbesparelse) , *Ref 3:*

Typer af Brændselsceller/(Elektrolyseceller)

| | AFC | PEMFC | SOFC |
|---------------------|-------------------------------|--------------------------------------|---|
| Electrolyte | Potassium hydroxide | Polymer membrane | Solid oxide |
| Catalyst | Nickel | Platinum | Perovskites/Ni |
| Operating temp. | 40–100°C | 60–200°C | 600 – 900 °C |
| Fuel(s) | H ₂ | H ₂ or CH ₃ OH | H ₂ , CO, NH ₃ , Hydrocarbons |
| Intolerant to | CO, CO ₂ | CO, S, NH ₃ | S |
| Electric efficiency | ~ 45 % | 40 – 55 % | 50 – 60 % |
| Applications | Mobile units, space, military | Mobile units, micro-CHP | CHP from micro-to large-scale |

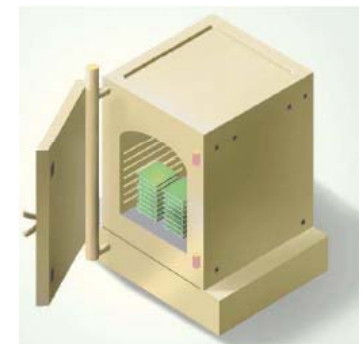
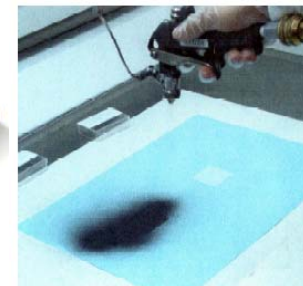
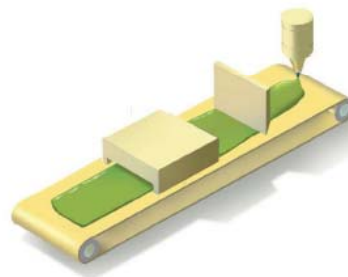
- R&D fokus: PEMFC, HT-PEM og SOFC
- Fordele og ulemper for alle
- Forskning og udvikling på alle spor på DTU (AEC elektrolyse)

SOFC Ni-YSZ supporteret celle



Ni/YSZ electrode
YSZ electrolyte
LSM-YSZ electrode

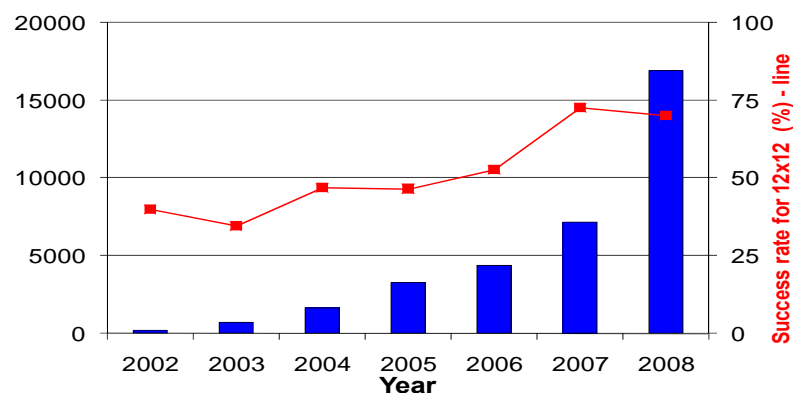
- Skalerbare fremstillingsmetoder



Samarbejde; DTU - Haldor Topsøe indenfor SOFC siden 1989



DTU Energy Conversion Department of Energy Conversion and Storage

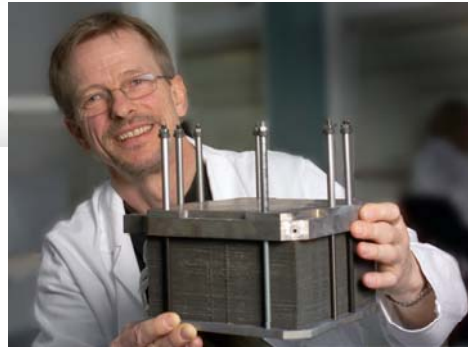


Datterselskab af Haldor Topsøe A/S Dannet 2004



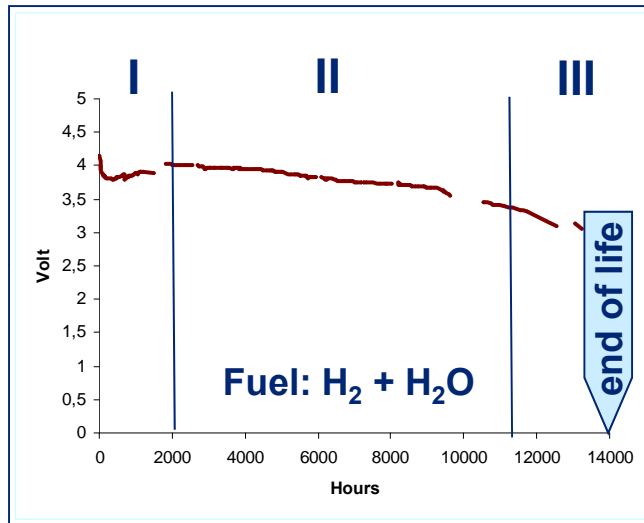
Teknologioverførsel fra DTU til TOFC

Stack test status



TOPSOE FUEL CELL 

2004



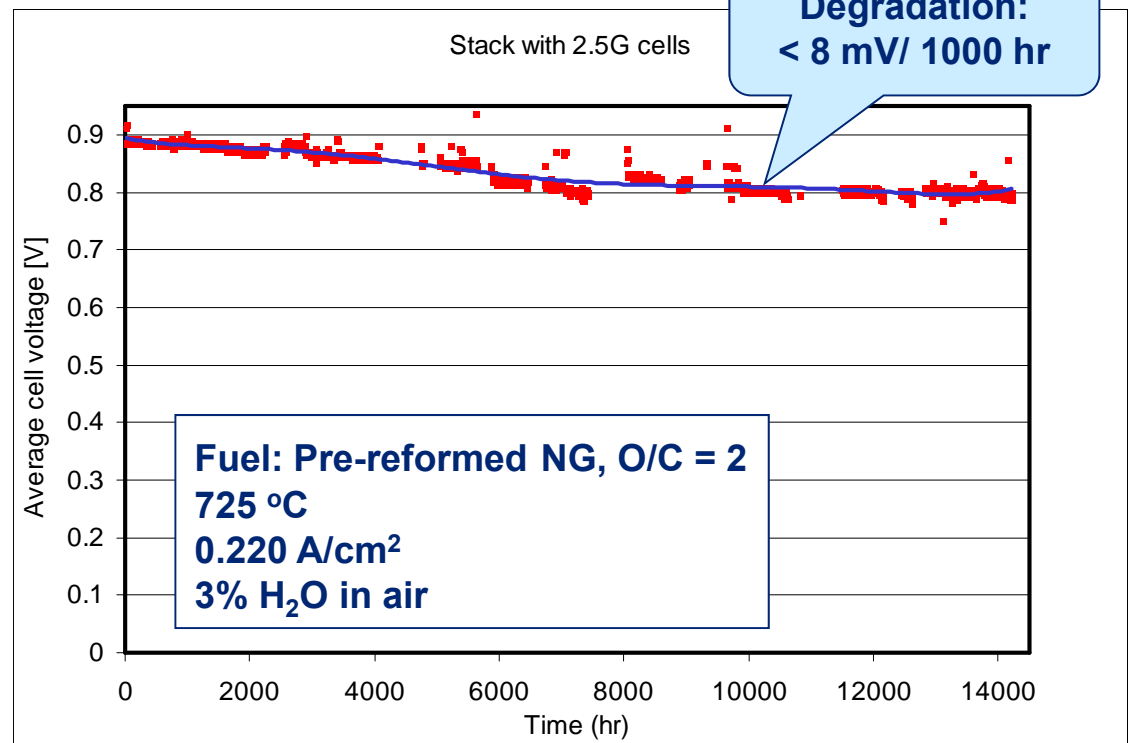
Test status:

14.000 hours

20 thermal cycles

Degradation steady/leveling off

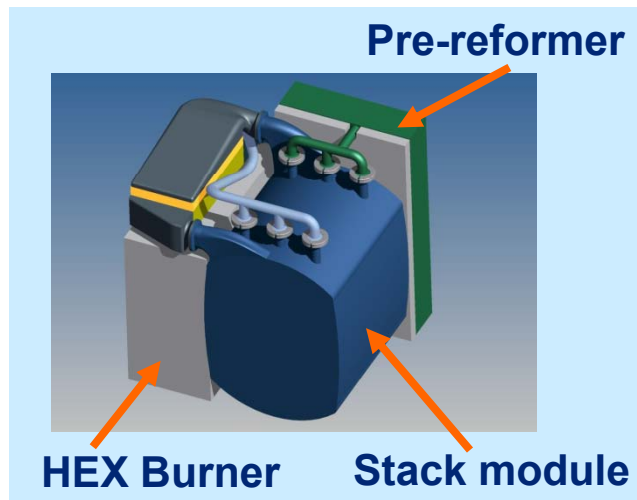
2011



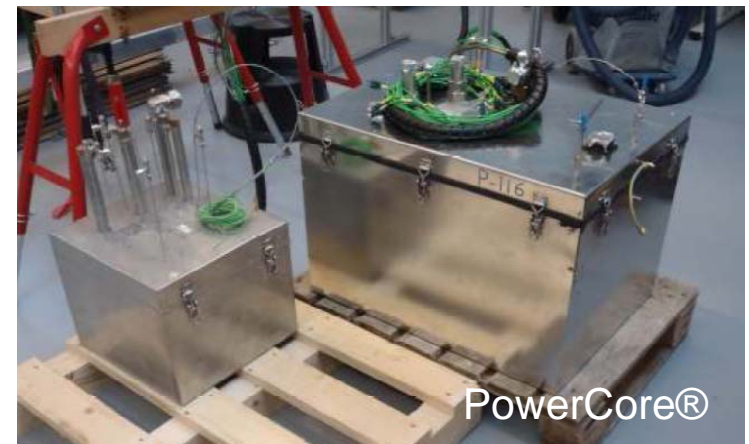
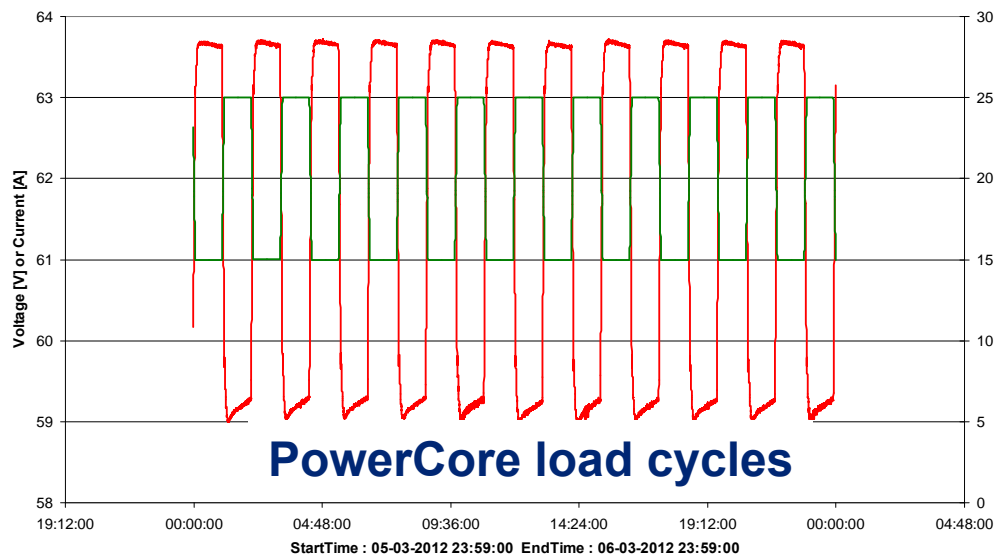
Source: Niels Christiansen, TOFC, Presented at 10 SOFC Forum 2012, Lucerne

μ-CHP PowerCore

TOPSOE FUEL CELL 



| PowerCore | Gen 2 | Gen 3 |
|------------------|-------------------|-------------------|
| DC power | 1.4 kW | 1.5kW |
| DC eff. (LHV) | 52% (80V, 18A) | 61% (59V, 25A) |
| Water evaporator | internal | external |
| Start-up burner | internal | external |
| Volumen | 148 L | 40L |
| Weight | 90 kg | 30 kg |



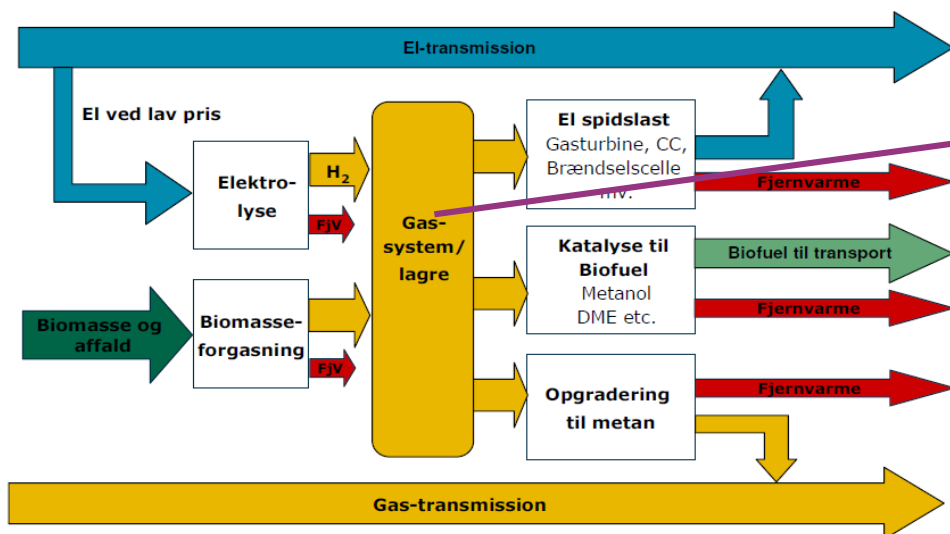
Source: Niels Christiansen, TOFC, Presented at 10 SOFC Forum 2012, Lucerne

Keramiske brændselsceller på markedet

- Japan: Kyocera, Osaka Gas, Toyota, mfl.
 - system til mikrokraftvarme introduceret april 2012
 - 700 W el, 42% virkningsgrad
 - pris ¥ 2.751.000 (ca. 200.000 kr.);
offentligt tilskud ¥ 1.000.000
- USA: Bloom Energy
 - decentral kraftproduktion til fx datacentre
 - 100 kW eller 200 kW el, ca. 50% virkningsgrad
 - alternative forretningsmodeller: købe strømmen,
men ikke anlægget



Brug af elektrolyse i fremtidens energisystem, SNG



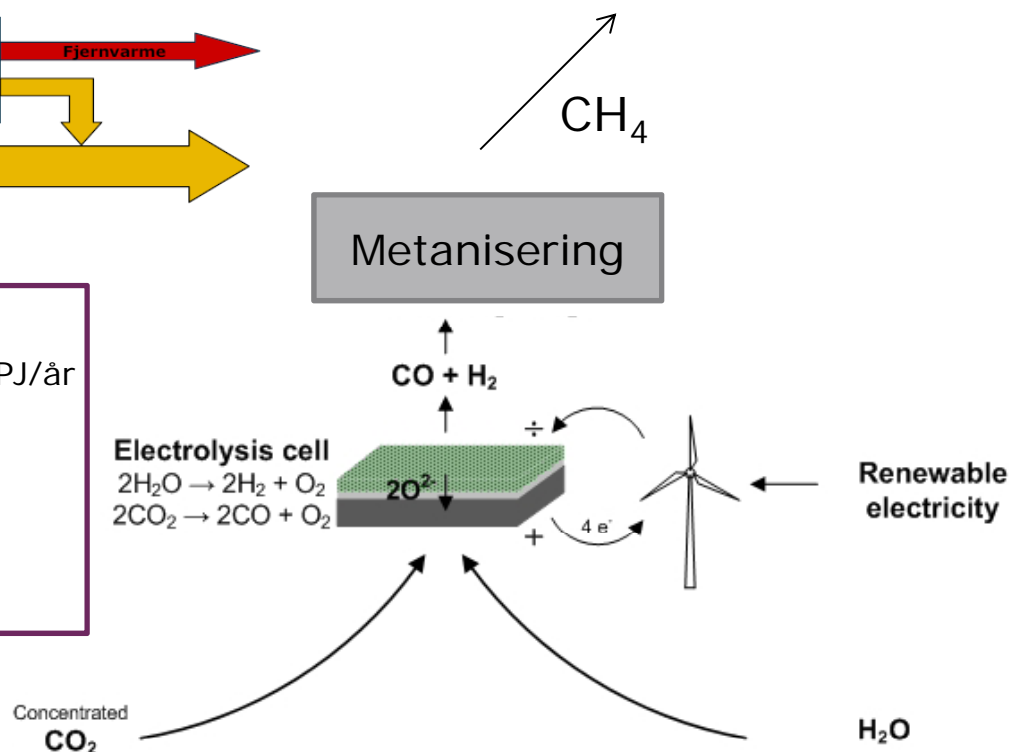
Energi 2050, Vindsporet, Energinet.dk

2050; (100 % VE)

+17GW Vind, +5 GW sol/bølge, BM; 200 PJ/år

Lagring;

- Gas: 11TWh, behov; 3.5 TWh
- EV. : 50 GWh, 1.5 mill EV, få timer

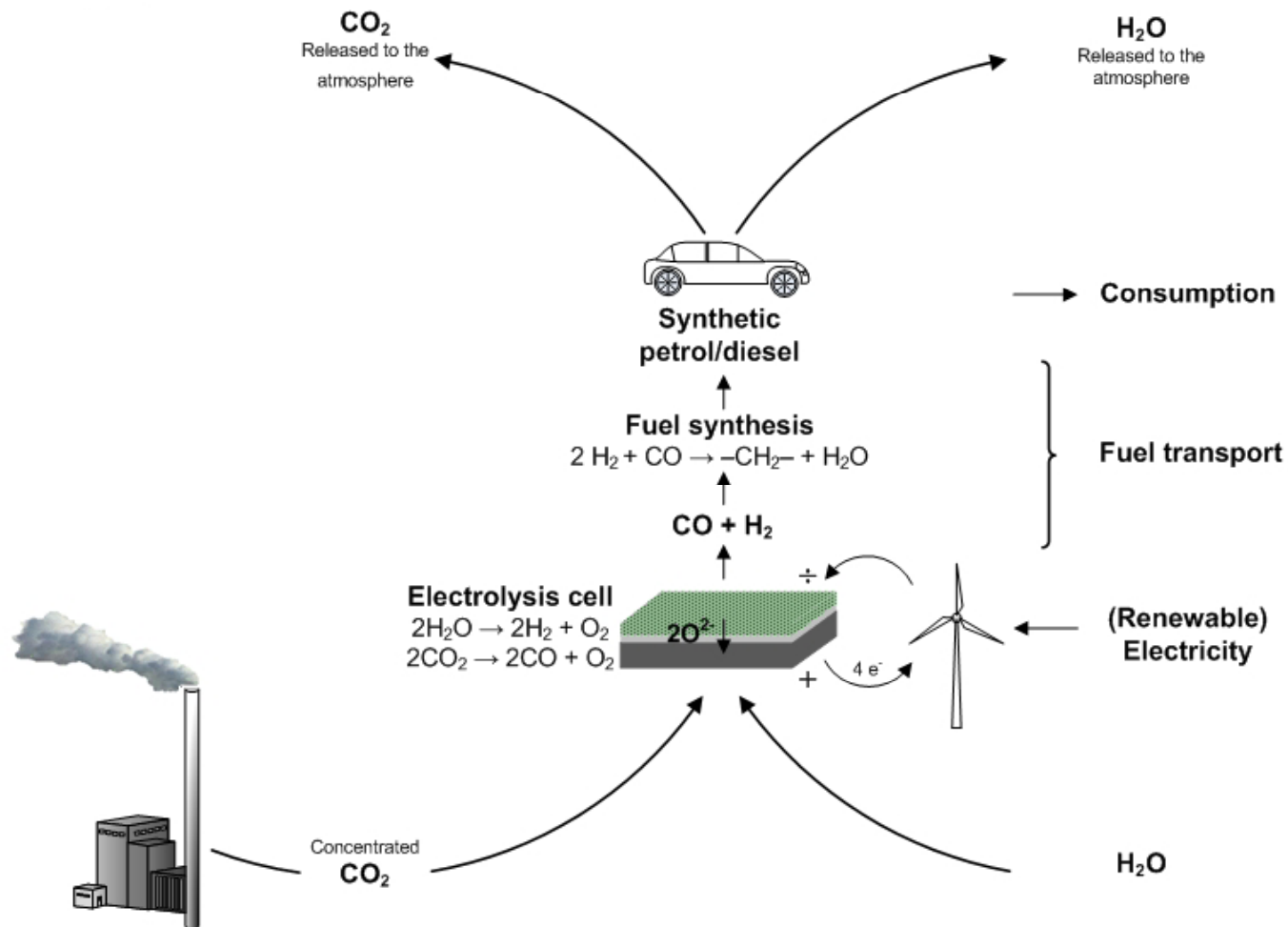


$$\eta_{\text{round_trip}} = \eta_{\text{electrolyse}} * \eta_{\text{brændselscelle}} = 95 * 55 \sim 50 \% \quad (\text{Via metan} \sim 40\text{-}45 \%)$$

Brug af elektrolyse i fremtidens energisystem

Syntetiske brændstof til transport

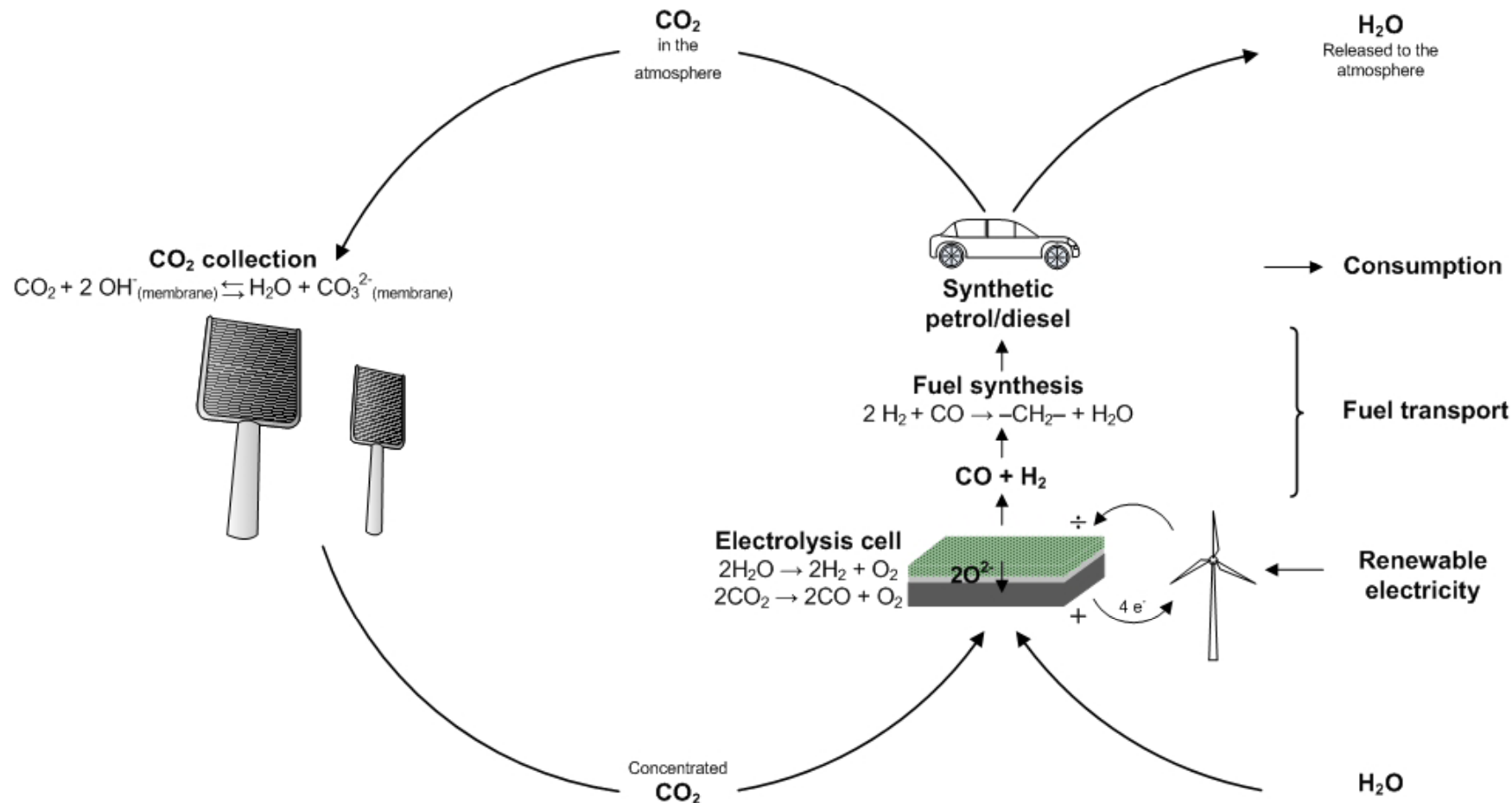
Short term realisation - CO₂ capture from industrial sources



Brug af elektrolyse i fremtidens energisystem

Syntetiske brændstof til transport

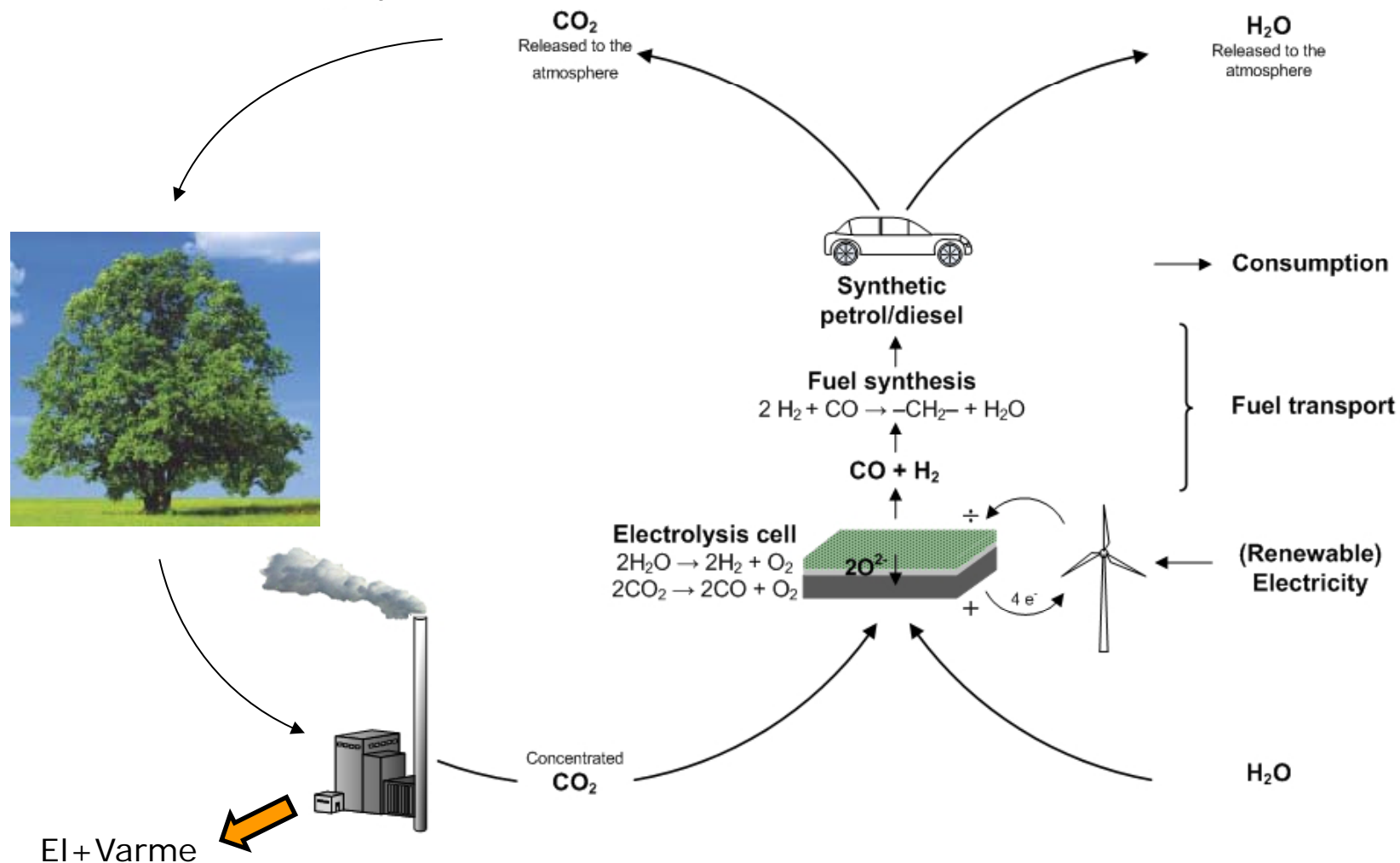
Long term realisation - CO₂ capture from the atmosphere



Brug af elektrolyse i fremtidens energisystem

Syntetiske brændstof til transport

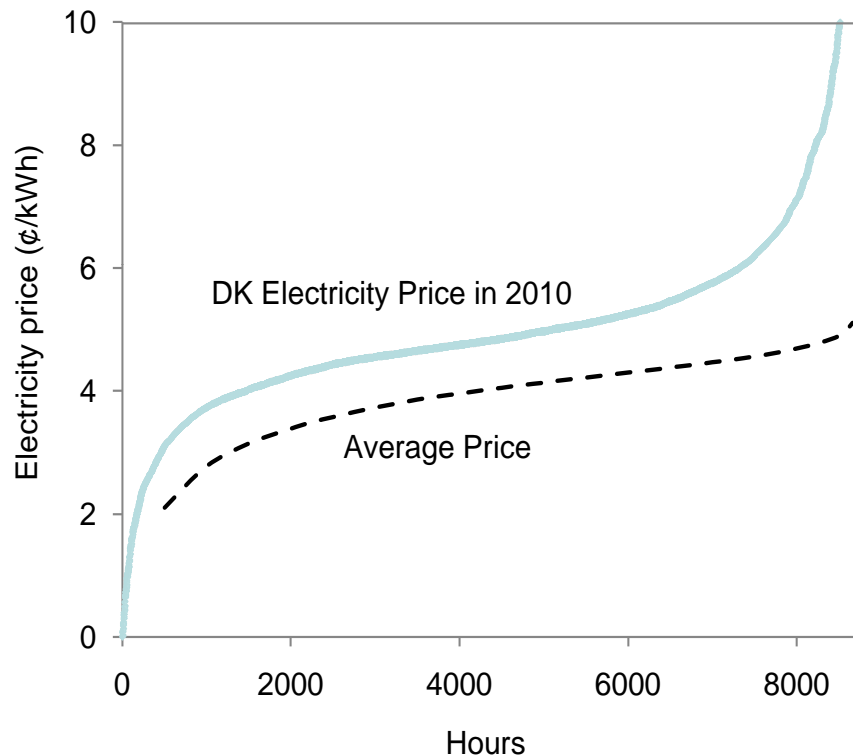
Opgradering af biomasse



Økonomisk analyse

100\$/kW*

Elektricitetspris



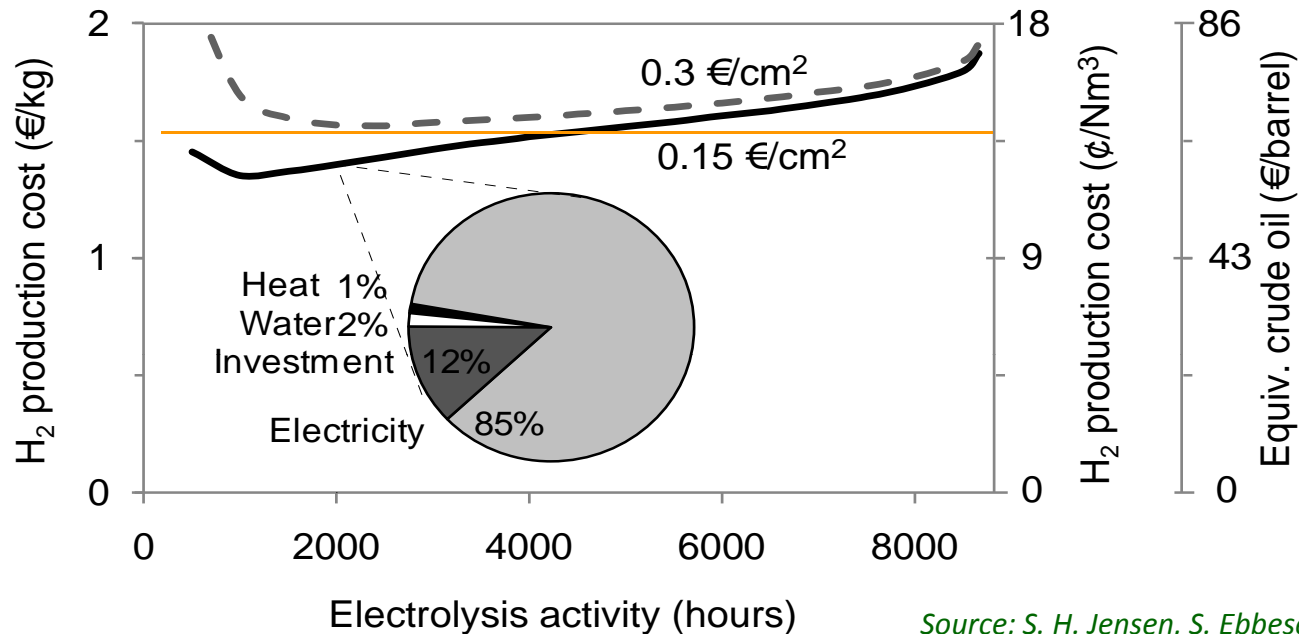
Andre antagelser

| | |
|---------------------------------|-----------------------------|
| SOEC system cost | 0.3 €/cm² |
| Heat | 0.23 ¢/kWh |
| Cell voltage (H ₂ O) | 1.3 V (V _{tn}) |
| Cell voltage (CO ₂) | 1.5 V (V _{tn}) |
| Current density | 1.5 A/cm² |
| Expected life time | 10 years |
| Interest rate | 5% |
| Expected CO ₂ cost | 23€/ton |
| Expected H ₂ O cost | 2.3 €/ton |

Source; S. H. Jensen, S. Ebbesen, K. V. Hansen, A. H. Pedersen[#]
and M. Mogensen, "Cost Estimation of H₂ and CO Produced by
Steam and CO₂ Electrolysis", 2011, (Unpublished).

*J. Thijssen, U.S. DOE/NETL 2007

Økonomisk analyse



Source; S. H. Jensen, S. Ebbesen, K. V. Hansen, A. H. Pedersen[#] and M. Mogensen, "Cost Estimation of H₂ and CO Produced by Steam and CO₂ Electrolysis", 2011, (Unpublished).

- Dagens oliepris ~ 85 \$/barrel

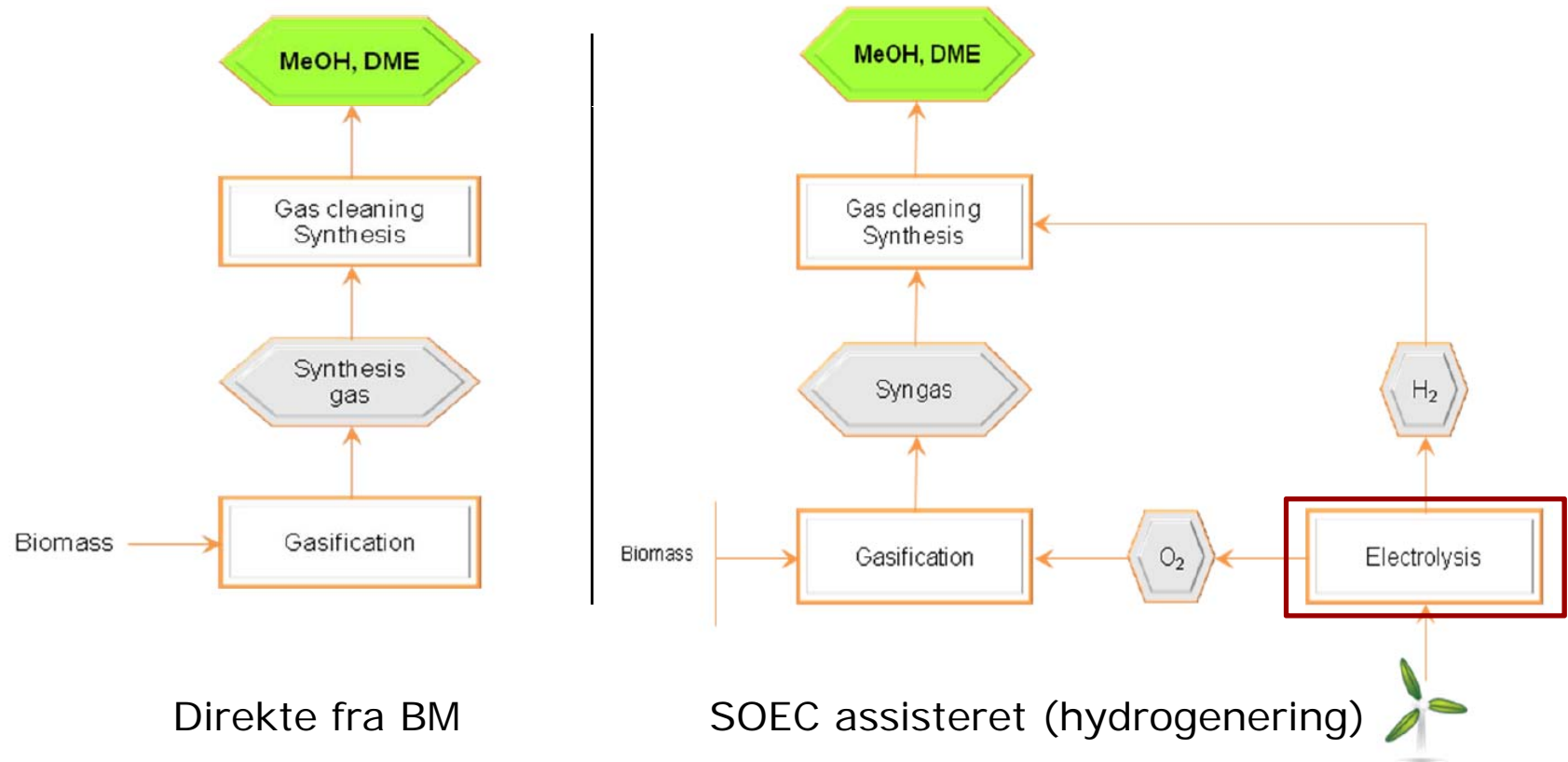
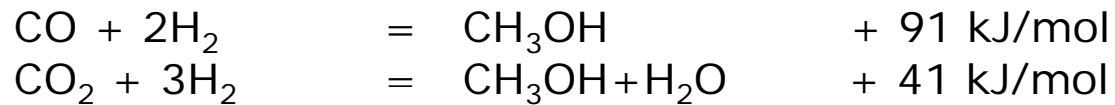
- 1.5 A/cm²
- 10 års levetid,
- 0.3 €/cm²



kræver fortsat udvikling !

Økonomisk analyse, Metanol fra træ

- "Green SynFuels", Final Project Report, EUDP 64010-0011.



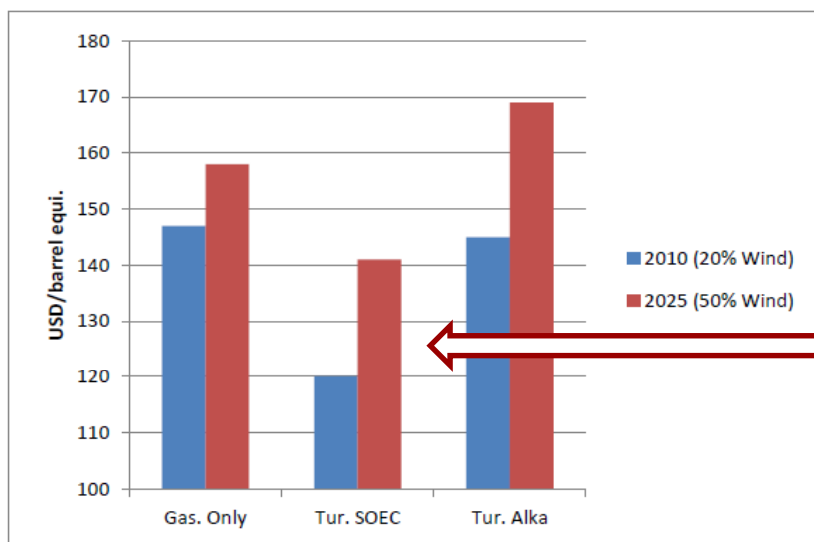
Økonomisk analyse, Metanol fra træ

| | Direkte | + SOEC |
|--------------|---------|--------|
| Træ | 207 MW | 207 MW |
| El | | 141 MW |
| Metanol | 121 MW | 243 MW |
| Effektivitet | 59,2 % | 70,8 % |

Kap. 6 John Bøgild Hansen, Haldor Topsøe A/S

Synergi

- Justering af C/H-forhold
- Termisk integration, Eksoterm+Endoterm proces



Kap. 3. Anders Korsgaard, Serenergy A/S

Økonomisk vurdering

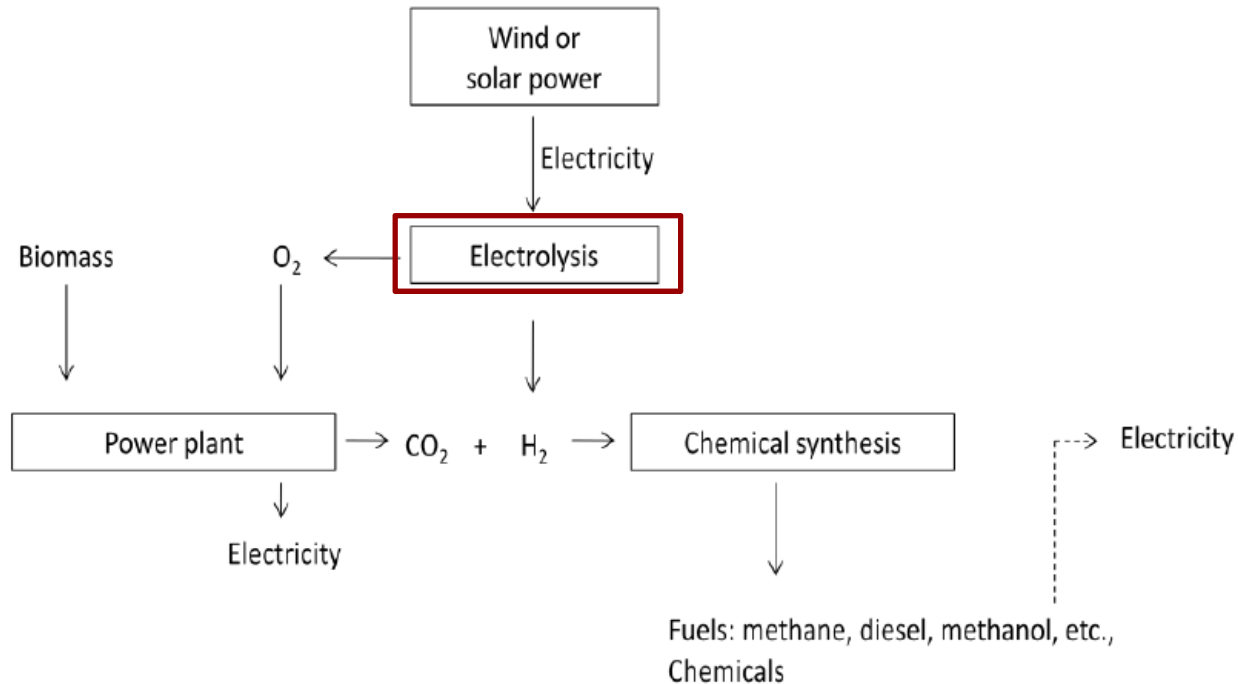
- Break even: 120 US\$/barrel

Source: Green SynFuels", Final Project Report, EUDP 64010-0011

John Bøgild Hansen, Mogens Mogensen, Allan Schrøder Petersen, Aksel Hauge Pedersen, Ivan Loncarevic, Martin Wittrup Hansen, Claus Torbensen, Jacob Bonde, Per Sune Koustrup, Anders Korsgaard, Jesper Lebak, Svend Lykkemark Christensen,

Project manager: Hans Over Hansen, Danish Technological Institute

Biomasse opgradering, Hydrogenering, CCR



- Biomasse er en begrænset ressource (~20% of behov)
- 100 PJ Biomass \longrightarrow 20 PJ Solid fuel + 50 PJ Liquid fuel, *Fermentering*
- 100 PJ Biomass + 150 PJ Hydrogen \longrightarrow 100 PJ Solid fuel + 130 PJ Liquid fuel *CCR*

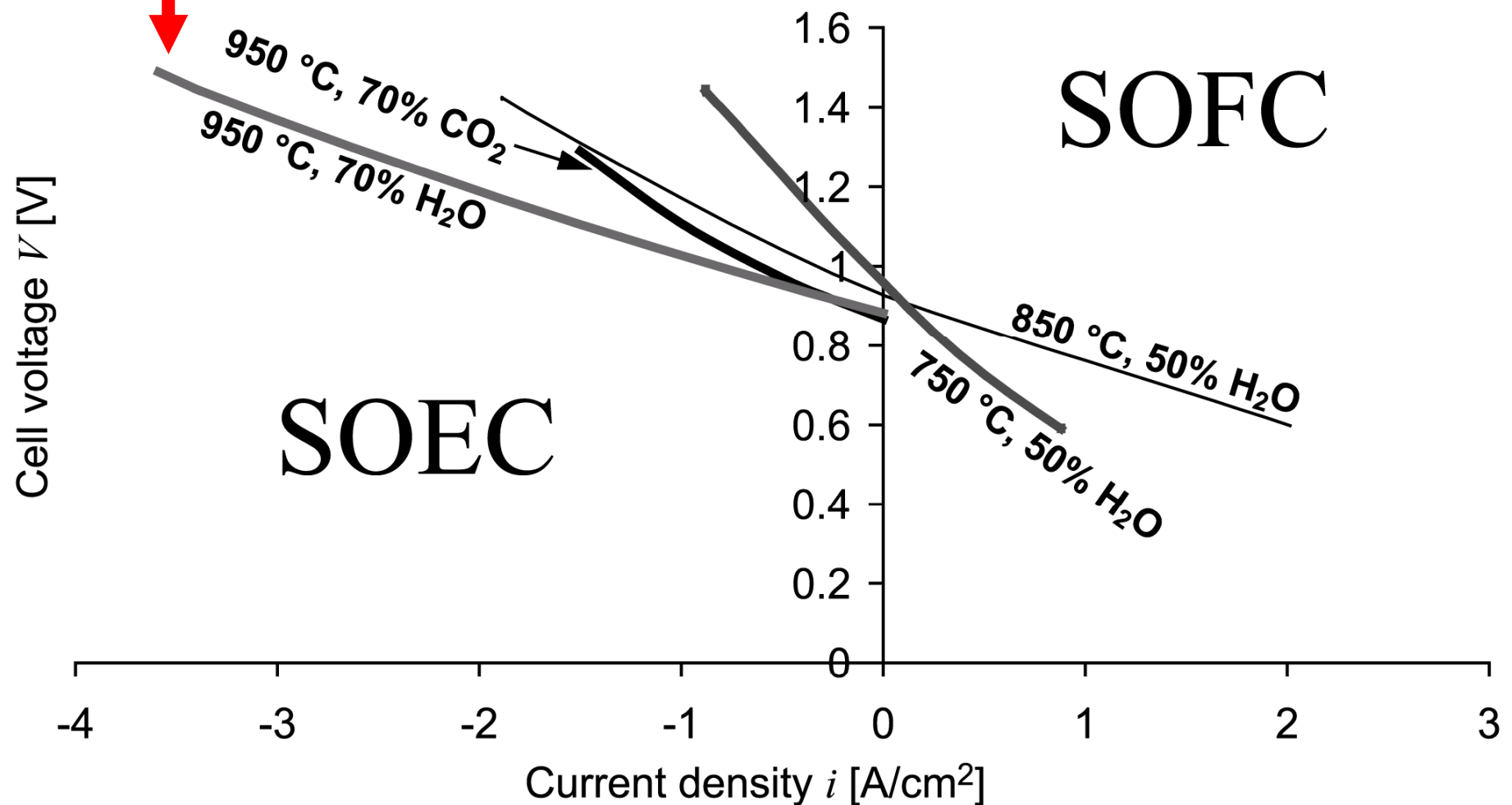
Source; H. Wenzel; "Breaking the biomass Bottleneck of the fossil free society", CONCITO, 2010

Olah G.A. "Beyond Oil and Gas: The methanol Economy", Angw. Chem. Int. Ed. 2005, 44, 2636

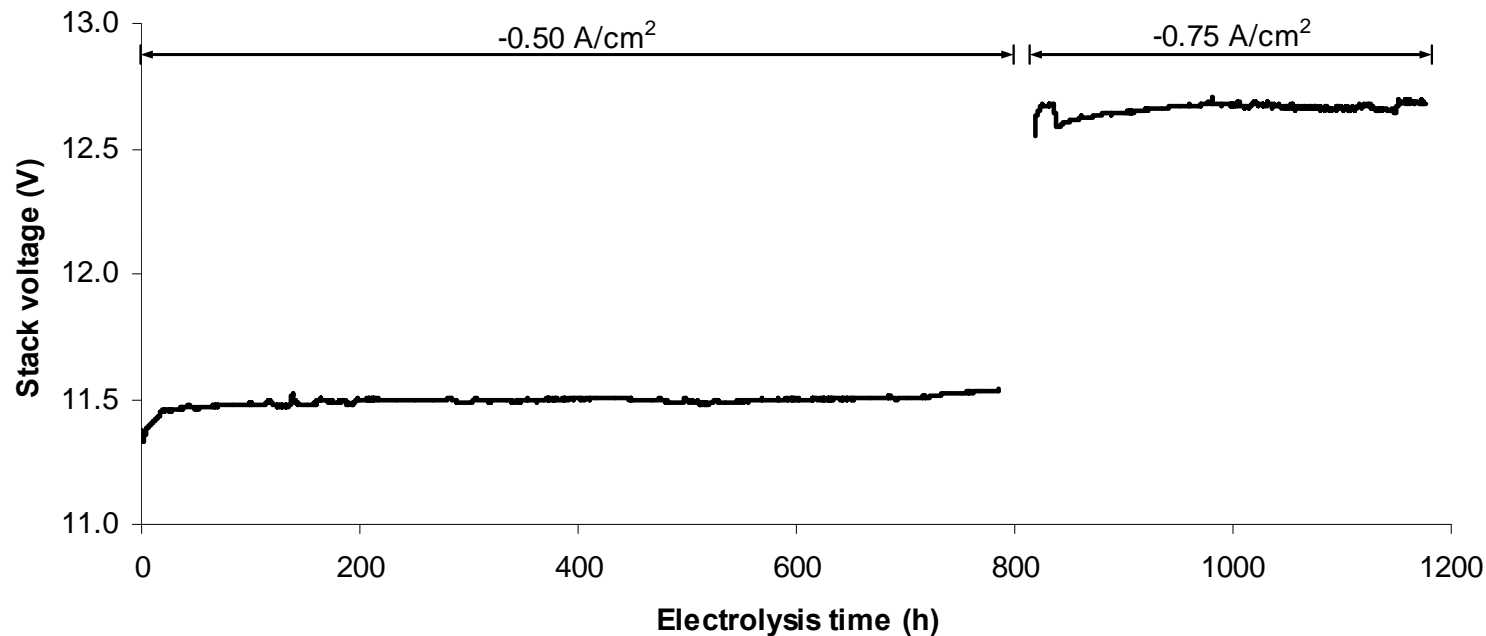
SOEC, Teknologistatus

World record !

[S. H. Jensen et al., International Journal of Hydrogen Energy, Volume 32, Issue 15, 2007, P. 3253](#)



Status på stak niveau



- Ydelsen er stabil ved moderat strømtæthed ($I \sim -0.75 \text{ A/cm}^2$ at 850°C)
- Standard TOFC stack, H_2O og co-electrolyse



- Reversible moduler (?), Produktionskapacitet eksisterer i DK,

Elektrolyse, AEC, PEMEC, SOEC

| Type | Largest system | Commercial suppliers | Danish companies |
|--------|----------------|--|--|
| AEC | 3.5 MW | Norsk Hydro Hydrogenics Iht,.... | Green Hydrogen Siemens Corp. Tech. (DK) |
| LT-PEM | 45 kW | H-TEC systems Hydro,... | IRD |
| SOEC | 15 kW | | Haldor Topsøe A/S TOFC |
| HT-PEM | W | | |






itet



Den første fuld skala Power2Gas anlæg (2MW, Hydrogenics) er under opførelse (E.ON.) i Falckenhagen, Tyskland (Lagring i naturgasnettet, 2013).

Resultater af systemanalyse, CEESA

Hvornår bliver der behov for elektrolyse ?

- 25 % Vindenergi kan indpasses uden forandringer
- > 25 %  Varmepumper, varmelagre [1]
- 40 – 45 %  El til transport, EV [2]
- >50 – 60 %  Syntetisk brændstof (transport) [1]

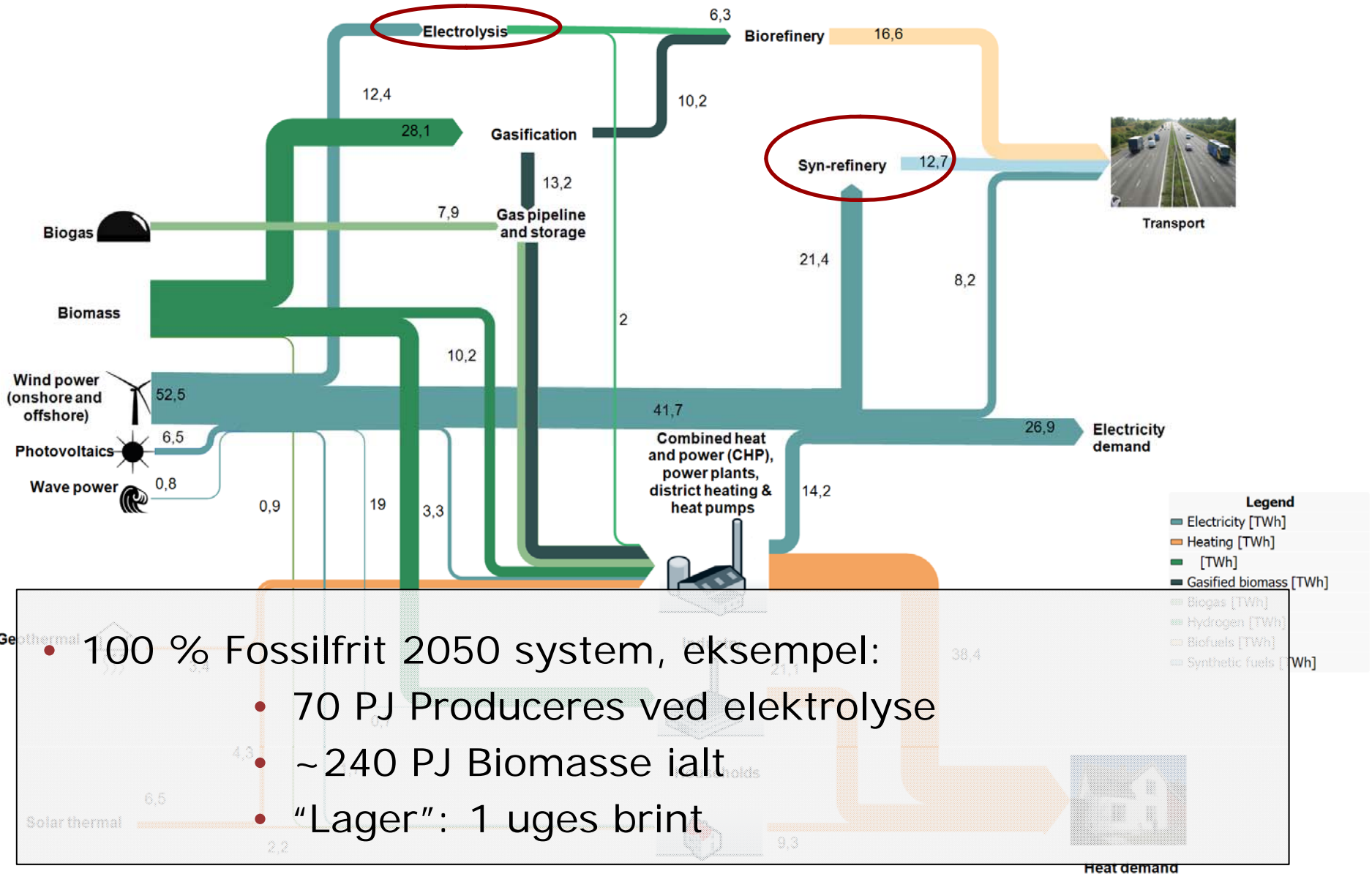
Referencer

[1] B. V. Mathiesen, "Fuel cells and electrolyzers in future energy systems",
Ph.D. Thesis, Aalborg University, 2008.

[2] Henrik Lund, Anders N. Andersen, Poul Alberg Østergaard, Brian Vad Mathiesen,
David Connolly, *Energy*, **42**, June 2012, P. 96

Resultater af systemanalyse, CEESA

Kilde: B.V. Mathiesen et al. "CEESA 100% Renewable Energy Scenarios towards 2050". Aalborg University, 2011. <http://www.ceesa.plan.aau.dk>. (to be published 2012).



- 100 % Fossilfrit 2050 system, eksempel:
 - 70 PJ Produceres ved elektrolyse
 - ~ 240 PJ Biomasse ialt
 - "Lager": 1 uges brint

Resumé, brændselsceller og elektrolyse i energisystemet

1. Øget andel af fluktuerende produktion
2. Biomasse er en begrænset ressource !
3. Flydende brændstoffer (Fly, tung transport) hvorfra ?



Brændselsceller:

- Høj virkningsgrad (også del-last) ➡ mere effektivt system



Elektrolyse, Syntetiske brændsler (Vind ➡ transport)



- Bedre udnyttelse af biomasse ➡ syn-fuel syntese, CCR
- Infrastruktur eksisterende
- Nærmere økonomisk analyse

Elektrolyse, (Power2Gas) Syntese gas, SNG



- Lagring af store mængder energi
- Infrastruktur eksisterende, flytning af store mængder energi

Acknowledgements

Sponsors

Danish Energy Authority



- Energinet.dk



- EU 

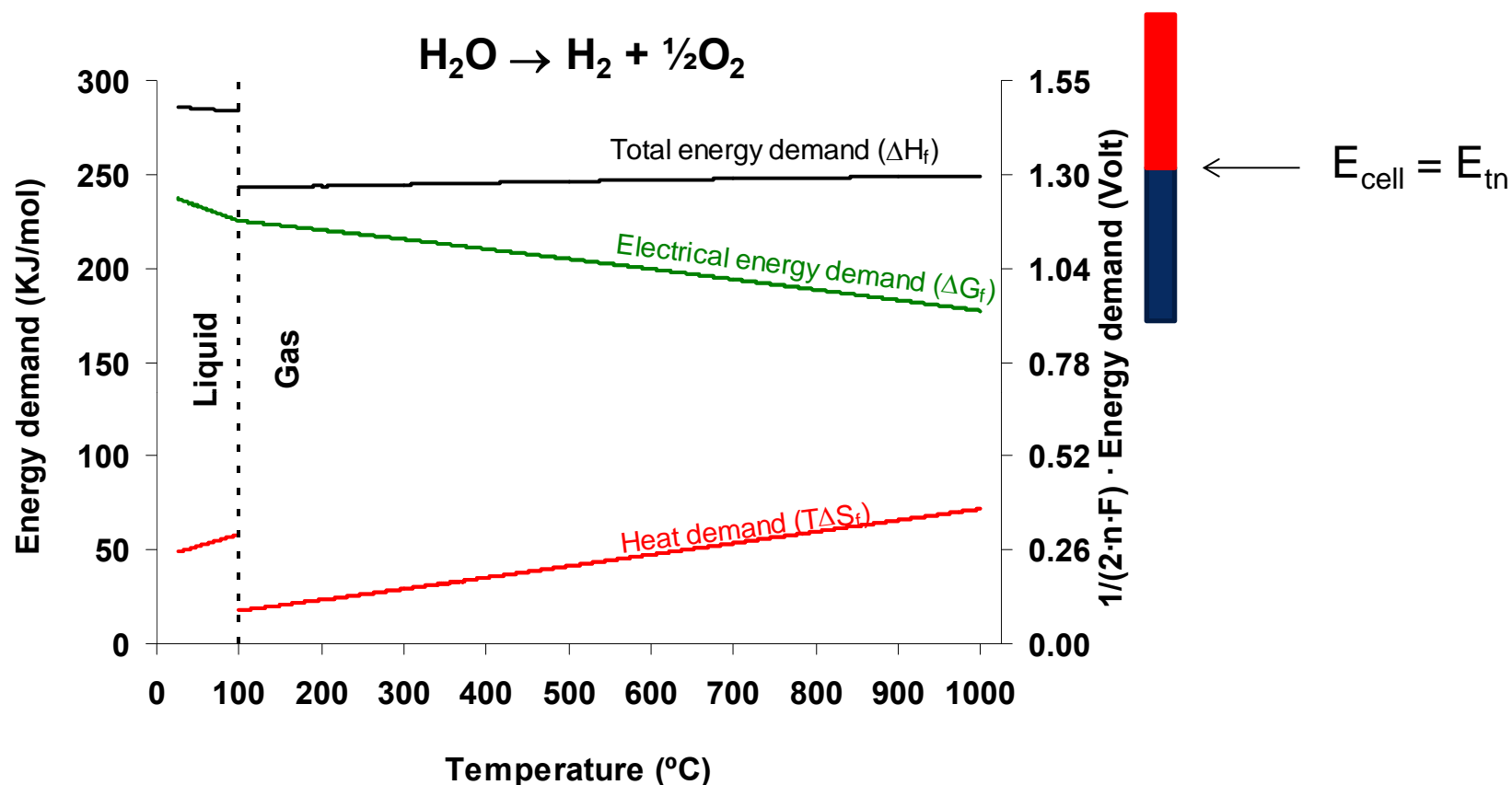
- Topsoe Fuel Cell A/S



- Danish Programme Committee for Energy and Environment
- Danish Programme Committee for Nano Science and Technology, Biotechnology and IT

Colleagues:

M. Mogensen, A. Smith, S. Højgaard Jensen, S. Ebbesen



$$\text{Energy ("volt")} = \text{Energy (kJ/mol)} / 2F$$

$$i \propto E_{\text{cell}} - \Delta G / 2F$$

$$E_{\text{tn}} = \Delta H / 2F$$

$$\text{Price} \propto 1/i \quad [\text{A/cm}^2],$$

$$\eta = \Delta H / \Delta G > 1, \quad \eta = 100 \% \text{ at } E = E_{\text{tn}} \text{ (no heat loss)}$$